

HYDROCARBON SOLVENTS FROM THE RESIN OF UNDERGROUND GASIFICATION OF ANGREN COAL

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Abstract. The article discusses the technology of coal production, its components, ways of using it as fuel. Mainly information is given on technologies of gasification of coal from Angren coal mine, and information on methods is also given.

Key words: coal, gasification, extraction, technological methods, raw materials

Coking resin can be used as a raw material for the production of hydroaromatic solvents.

The resources of raw materials for valuable solvents can also be expanded at the expense of those quantities of underground coal gasification (UCG) tar, which will be obtained under the condition of industrial implementation of underground gasification of Angren coals. The properties and chemical composition of resins for semi-coking and underground coal gasification are identical. This allows the development of a number of similar processes based on them.

In contrast to semi-coking resin, CCGT resin was subjected to heat treatment at the first stage under a hydrogen pressure of 40 atm. and a temperature of 400°C. The experiments were carried out on a laboratory microinstallation with a reactor volume of 20 ml.

№	Resin Sample Characteristic	
1	Density at 20°C, g/cm ³	1,0343
2	Relative molecular weight	213
3	Viscosity at 50 °C, m ² /s (eat)	18,5.10 ⁻⁶ (18,5)
4	The amount of insoluble substances in C ₆ H ₆ , %	0,26
5	Ash content, %	0,055
Fractional composition, %:		
1	distillation to 100°C	2,7
2	100 — 200°C	4,5

3	200 — 250°C	25,0
4	250 — 300°C	18,5
5	remainder above 300°C	49,3

Thermal hydrogenation contributed to the production of a product in which the content of aromatic hydrocarbons increased from 32% to 76.5%. The yield of the hydrogenate in the optimal experiment at a space velocity of 1.5–2.0 h⁻¹ was 95%. Hydrogenate fraction 200–300°C was isolated by distillation, which was subjected to hydrogenation on a nickel-molybdenum catalytic system at 300°C, space velocity 0.5 h⁻¹, pressure 50 atm, and hydrogen molar concentration 7:1. The composition and properties of the hydrogenation feedstock, the conditions for an optimal hydrogenation experiment, and the characterization of the hydrogenation product are given above.

The composition and properties of the feedstock for the production of solvents

Density at 20°C, g/cm ³	1,0238
Index of refraction, n_d^{20} at 20°C	1,5820
Drum index coefficient. Z	36
Viscosity, m ² /s (cst)	13,2 · 10 ⁻⁶ (13,2)
Relative molecular weight	171
Iodine number mg ioa/100 g	31,14
Amount of sulfonated hydrocarbons %, mass	97,5

Boiling limits, °C: H. κ – 223; 10% - 235; 20% - 247; 30% - 255; 50% - 280; 70% - 288; 80% - 298, 92% - 300.

Conditions for an optimal hydrogenation experience and characterization of the hydrogenate:

1	Catalyst	“Nickelmolybdenum system”
2	Temperature, °C	300
3	Volumetric velocity, ch ⁻¹	0,5
4	Yield of hydrogenate, % mass.	92
5	Hydrogen consumption, %	1,4
6	Hydrogenizate viscosity, m ² /s (cst)	6,2 · 10 ⁻⁶ (6,2)
7	Density at 20°C, g/sm ³	0,9222
8	Relative molecular weight	189
9	Refractive index, n_d^{20} at 20°C	1,4993
10	Iodine number, mg iodine/100 g.	15,5

The data show that the hydrogenation process contributed to a significant decrease in the viscosity of the product, saturation of unsaturated hydrocarbons. The results of narrow fractionation, the data of which are given in table. 1 show that the hydrogenation process made it possible to obtain not only medium-boiling, but also some low-boiling hydrocarbons. The values of the index of refraction of the isolated

fractions indicate the content of predominantly hydroaromatic hydrocarbons in them. The absence of pure samples of hydrogenated hydrocarbons and their homologues did not allow us to characterize these fractions in more detail [1].

Table 1 - Results of narrow fractionation of pyrocondensate after hydrofinishing

Boiling limits, °C	Exit %	Refractive index при 20°C	Boiling limits, °C	Exit, %	Refractive index при 20°C
Н.к.87,6	-	-	196,7-204,6	1,3	1,4880
87,6-100,7	2,7	1,4392	204,6-208,6	-	-
100,7-107,6	-	-	208,6-209,6	1,5	1,4900
107,6-109,6	1,3	1,4340	209,6-212,6	2,8	1,4910
109,6-122,8	-	-	212,6-220,7	-	-
122,8-136,0	3,7	1,4350	220,7-221,7	3,2	1,4930
136,0-143,4	1,1	1,4403	221,7-222,7	-	-
143,4-144,0	-	-	222,7-225,7	2,6	1,4960
144,0-146,0	2,3	1,4480	225,7-227,7	-	-
146,0-162,7	-	-	227,7-232,7	5,3	1,5010
162,7-164,7	1,3	1,4570	232,7-239,9	-	-
164,7-165,0	-	-	239,9-244,0	8,2	1,5060
165,0-168,5	2,9	1,4603	244,0-246,6	-	-
168,5-174,5	-	-	246,6-251,6	5,3	1,5120
174,5-177,5	2,7	1,4640	Remainder above 251,6	37,0	-
177,5-185,2	8,0	1,4710			
185,2-194,7	-	-	Static delay + loss	3,1	-
194,7-196,7	3,7	1,4815	-	3,1	-

Of interest is the fact that the entire resin of underground coal gasification was used as a raw material, without preliminary separation of phenols and bases from it. The economic feasibility of the technology for obtaining hydroaromatic hydrocarbons during the processing of resin is indisputable. It eliminates the inevitable loss of part of the raw material during its dephenolization and depyridination.

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